## **ERRATUM**

Volume 135, Number 2 (1992), in the article "Piperidine Hydrogenolysis on a Commercial Hydrocracking Catalyst. III. The Effects of Zeolite Unit Cell Size, Catalyst Sulfur Content, and Coke Deposition on Catalyst Activity and Deactivation," by G. C. Hadjiloizou, J. B. Butt, and J. S. Dranoff, pages 481–504: Equation (5) of the paper should read

$$r_i = k_i^{\text{o}} C_1^2 s_i = \frac{k_i^{\text{o''}} K_{\text{pip}_i}^2 C_1^2 s_i}{(1 + K_{\text{pip}_i} C_{1_o})^2}.$$
 (5)

Reference (10) should read

10. Hadjiloizou, G. C., Butt, J. B., and Dranoff, J. S., J. Catal. 135, 27 (1992).

The following Nomenclature section was inadvertently omitted.

## **NOMENCLATURE**

$a_i$	Decay parameter for the formation of product $i$ , min <sup>-0.5</sup> .	$k_{d_t}^*$	Apparent rate constant of overall deactivation reaction, min <sup>-1</sup> .
$C_1$	Concentration of piperidine, g mol/liter.	$k_i$	Reaction rate constant of formation of product <i>i</i> .
$C_{1_0}$	Initial concentration of piperidine, g mol/liter.	$k_i^{\text{o}}, k_i^{\text{o"}}$	Initial reaction rate constants of formation of product <i>i</i> , liter <sup>2</sup> /
D	Average deviation, defined as $D = (1/m) \sum_{m} \{[ k_{i,\text{obs},m}^{om}  -$		g mol/g cat/min and g mol/g cat/min, respectively.
$E_{d_t}$	$k_{i,\text{pred},m}^{o"} J/k_{i,\text{obs},m}^{o"}\} \times 100.$ Activation energy of overall deactivation, kcal/g mol.	$k_{ij}^{*\prime}$ , $k_{ij}^{o"}$	Rate constants of formation of product $i$ on catalyst $j$ , as defined in Eq. (6).
$F_{\mathfrak{1}_0}$	Reactor inlet molar flow rate of piperidine, g mol/min.	$k_t^{\rm o}$	Initial rate constant of overall reaction, liter <sup>2</sup> /g mol/g cat/min.
i	Index: $i = 2 = N$ - $n$ -pentylpiperidine, $i = 3 = 2$ - $n$ -pentylpiperidine, $i = 4 = decahydro-$	$N_{ij}^{ m o}$	Initial total number of sites active for formation of product <i>i</i> on catalyst <i>j</i> .
<i>K</i> .	quinolines. Adsorption equilibrium constant	n*	Order of concentration dependency of deactivation.
$K_{pip_i}$	for piperidine associated with	pip	Piperidine.
	formation of product i, liter/	R	Gas constant, kcal/g mol/K.
$K'_{\mathrm{pip}_i}$	g mol. Preexponential factor of $K_{pip_i}$ , li-	$R^2$	Coefficient of determination for regression analysis.
Pip <sub>i</sub>	ter/g mol.	$r_i$	Reaction rate of formation of
$k_{d_i}$	Rate constant of overall deacti-		product i, g mol/g cat/min.
•	vation reaction, liter/g mol/min.	$s_i$	Activity of catalyst at time on stream t for formation of prod-
$k'_{d_t}$	Preexponential factor of $k_{d_t}$ , liter/		uct i.
	g mol/min.	T	Absolute temperature, K.

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t	Time on stream, min.	$x_t^0$ Initial total conversion of piper-
W	Weight of catalyst, g.	idine.  Greek Symbols
$X_i$	Conversion of piperidine to product <i>i</i> at time on stream <i>t</i> .	$\Delta H_{\text{pip}_i}$ Enthalpy change of adsorption of piperidine associated with formation of product $i$ , kcal/g mol.
$X_i^{0}$	Initial conversion of piperidine to product <i>i</i> .	
$X_t$	Total conversion of piperidine at time on stream t.	7 Space time = $WC_{1_o}^2/F_{1_o}$ , g mol · g cat · min/liter <sup>2</sup> .